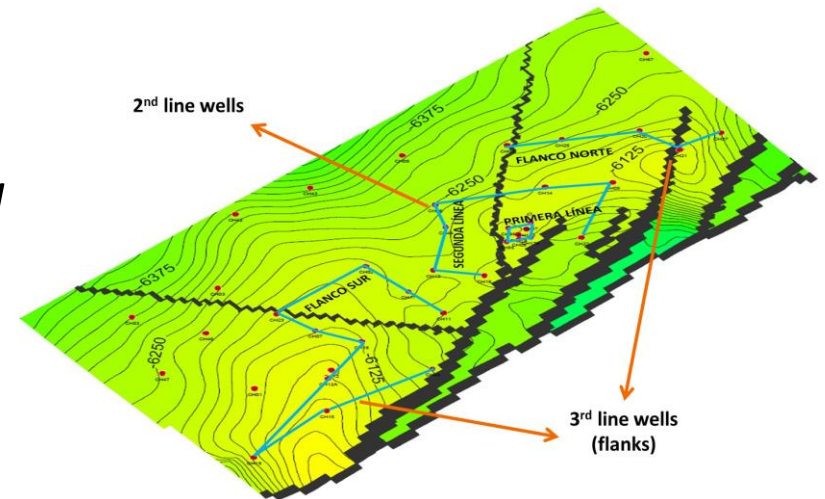
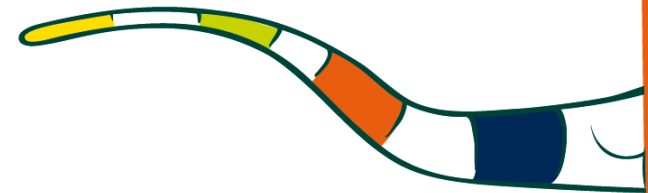


POSIBILIDADES Y RETOS PARA LA COMBUSTIÓN IN SITU EN COLOMBIA

*Universidad Nacional de Colombia
Facultad de Minas
2017*



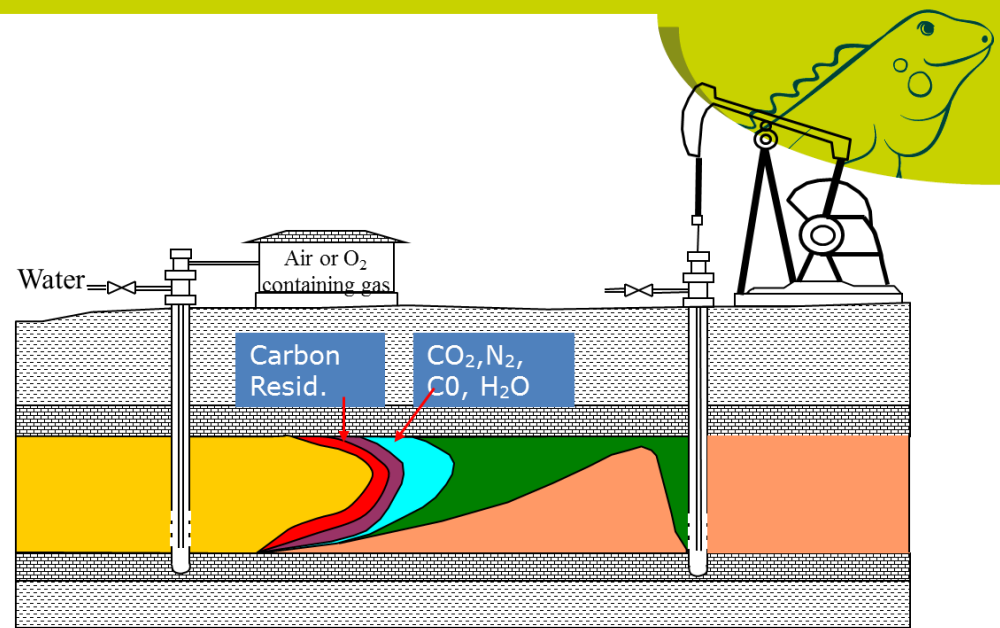
EIDER NIZ VELÁSQUEZ
LÍDER DE ÁREA DE CONOCIMIENTO EOR, ICP









Outline

- In situ Combustion
- The Chichimene ISC Pilot
 - History
 - Current Status
- Laboratory Studies
- Nitrogen Connectivity Test
- Challenges and Future Activities





- | | | | |
|---|----------------------------|---|-------------------------|
|  | Burned Zone |  | Steam Zone |
|  | Combustion Zone |  | Altered Saturation Zone |
|  | Cracking/Vaporization Zone |  | Native Reservoir |

COMBUSTIÓN IN SITU

In-Situ Combustion

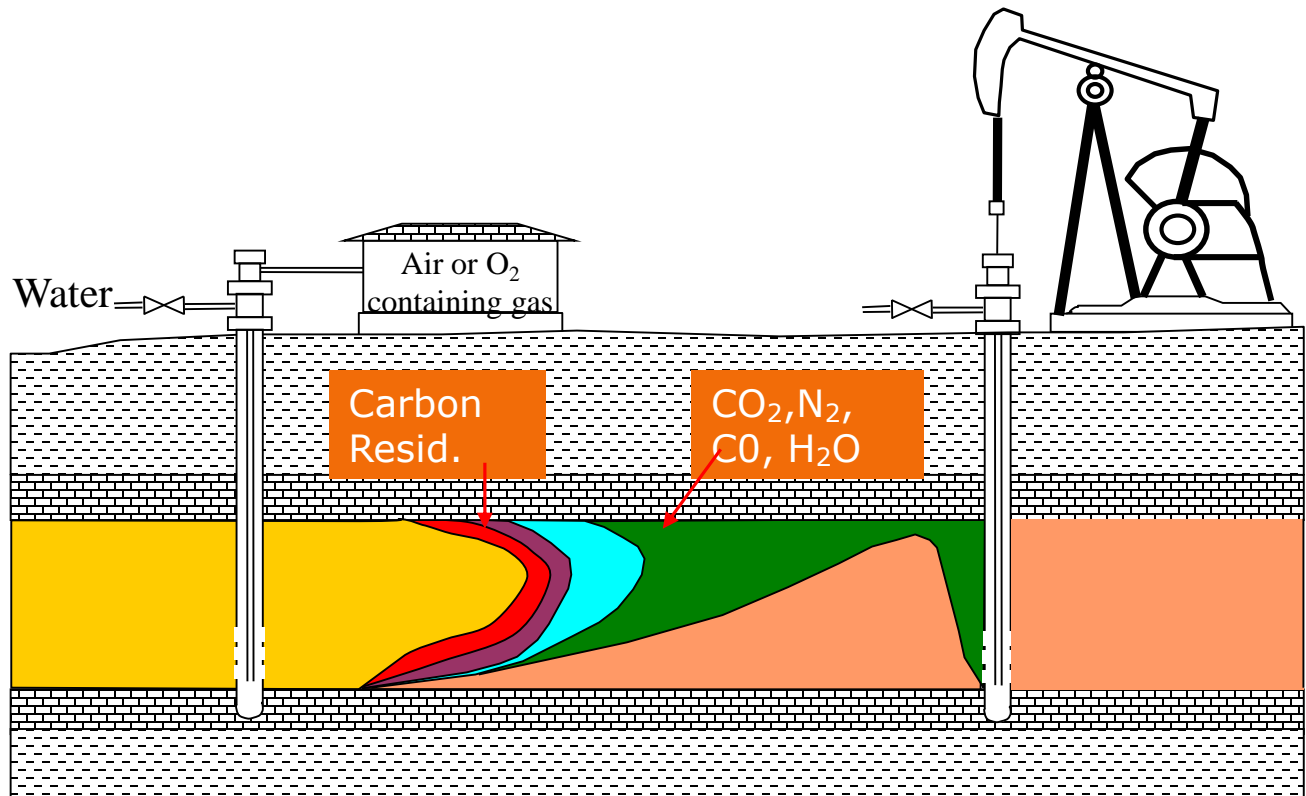








Inject Air or Oxygen

- Advantages:
 - Heat generated in-situ
 - No surface/wellbore heat losses
 - Fewer limitations on depth
 - Not dependent on latent heat
 - Fewer pressure constraints
 - Fuel used is residual OIP (usually 5 – 10% of OIIP is consumed)
 - Not dependent on water source
 - Applicable to thin reservoirs
- Disadvantages:
 - Difficult to control
 - Can result in well loss or damage
 - Produces combustion products
 - N_2 , NO_x , if air is injected
 - CO_2
 - Various environmentally-unfriendly products
 - HSE risk if O_2 breaks through (auto-ignition risk if $O_2 > 9$ mole%)
 - HSE risk – air compression
 - Gas treatment of produced solution gas mixed with flue gases



“Classical” In Situ Combustion Process Schematic



- | | | | |
|---|----------------------------|---|-------------------------|
|  | Burned Zone |  | Steam Zone |
|  | Combustion Zone |  | Altered Saturation Zone |
|  | Cracking/Vaporization Zone |  | Native Reservoir |

Propiedades de Yacimiento – Principales Proyectos



Campo, País	Formación	Buzamiento	Profundidad (ft)	Temperatura de yacimiento (°F)	Espesor neto (ft)	Porosidad (%)	Saturación de Agua irreducible (%)	Saturación de aceite al inicio CIS (%)	Permeabilidad (mD)
Suplacu de Barcau, Rumania	S	5- 8	115-720	65	20- 89	32	15	<85	5000-7000
Balol, India	S	4-7	3280	158	9-50	28	30	70	3000-8000
Santhal, India	SS	3-5	3280	158	9-50	28	30	70	3000-5000
Bellevue, Lousiana, USA	SS	0-5	400	75	10-83	32	27	73	650

Campo, País	Viscosidad del crudo (cp)	Gravedad (°API)	P inic/ P. inicio CIS (psi)	OOIP (MMbbl)
Suplacu de Barcau, Rumania	2000	16	140 / 80	310
Balol, India	100-450	16	1450 /1450	128
Santhal, India	50-200	18	1450 /1450	300
Bellevue, Lousiana, USA	676	19	/ 40	4.6 ;10.6

Fuente: TURTA A, et al. Current status of comercial in situ combustion projects worldwide. Journal of Canadian petroleum technology.

Resultados de los Principales Proyectos

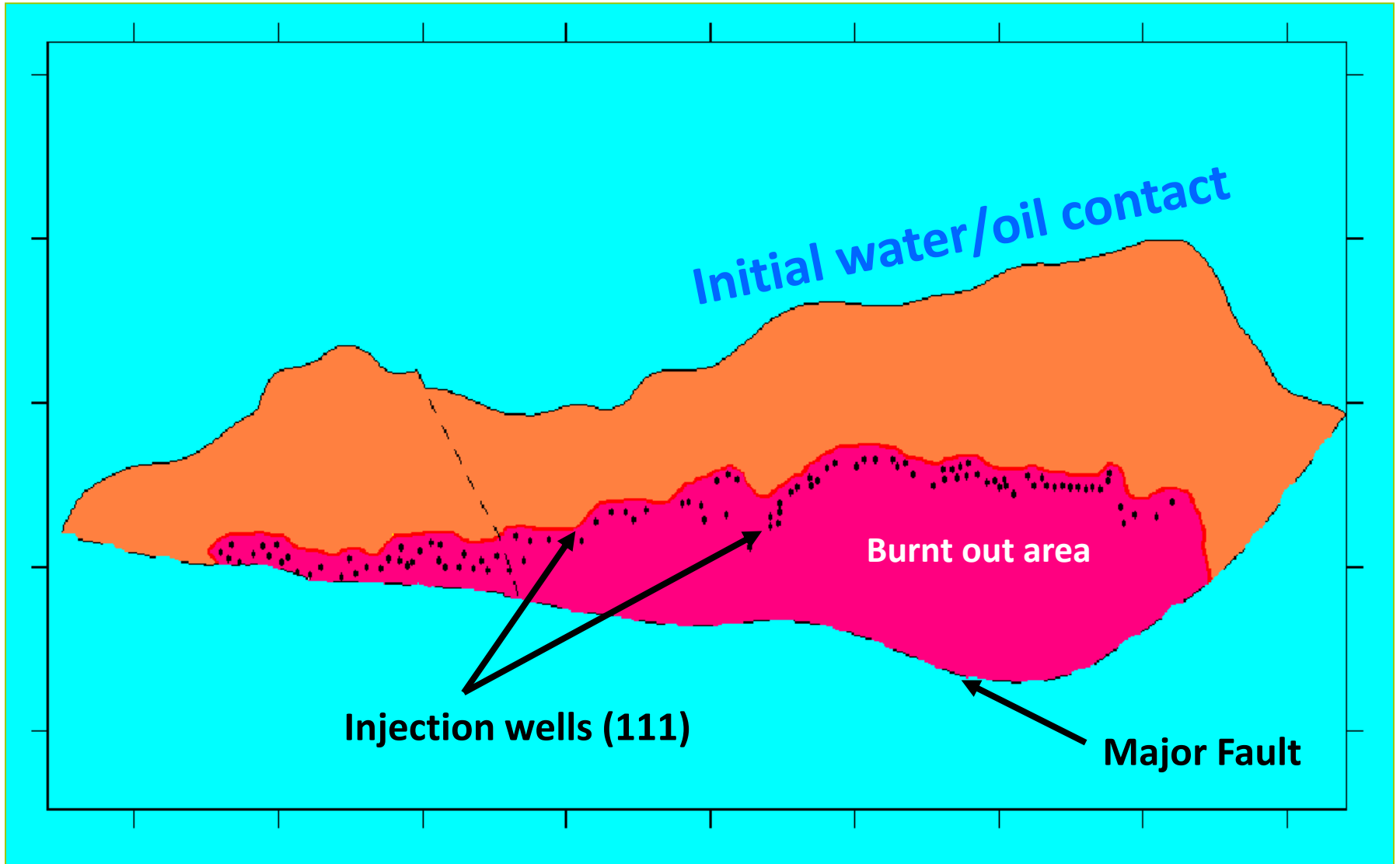


Campo, País	Fecha (inicio de operación)	Presión inyección (psi)	N de pozos inyectoros	N de pozos productores	Producción diaria con ISC (Bbl/día)	Corte de agua (%)	Utilización de O ₂ (%)	Relación aire/crudo (scf/bbl)	Recobro esperado de crudo (%)
Suplacu de Barcau, Rumania	1971	150- 200	111+	736+	9000++	82	95	14000	52
Balol, India	1997	1300- 1600	30	75	4400	60	>95	5600	38
Santhal, India	1997	1200-1500	30	105	4000	60	>95	5600	36
Bellevue, Lousiana, USA	1970	60	15	90	300	90	80	15000	60

+ 24 de los pozos fueron estimulados bajo inyección cíclica de vapor (CSS)

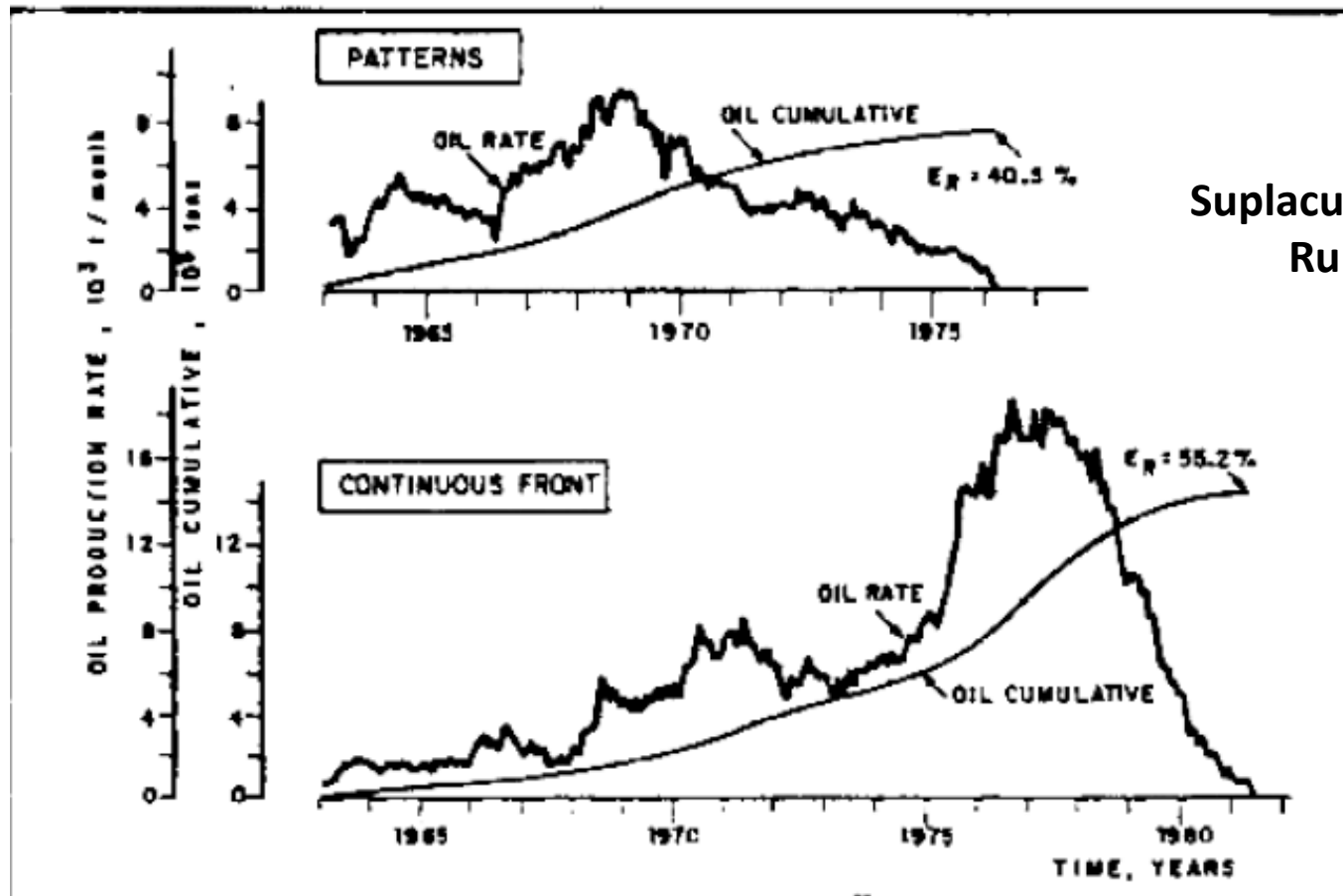
Fuente: TURTA A, et al. Current status of comercial in situ combustion projects worldwide. Journal of Canadian petroleum technology.

Suplacu de Barcau. Position of the combustion front as of July 1st, 2004





Patterns bad line drive good



Suplacu de Barcau,
Rumania



Suplacu: Essential Results/Problems

Results

- ❑ Ultimate oil recovery: >50%
- ❑ AOR in the range of 6,000 to 18,000 scf/bbl (1,000 – 3,000 sm^3/m^3), increasing in time
- ❑ At the low inj. pressure., even the AOR of 18,000 scf/bbl is economical
- ❑ Water cut increased slowly, up to 82%

Operational Aspects

- ❑ Burning out of some producers
- ❑ Hot well workover challenges; special killing drilling mud needed
- ❑ Dehydration/desalting coupled with a stripping unit for processing of crude oil
- ❑ Leakage to the surface of some combustion gases/air

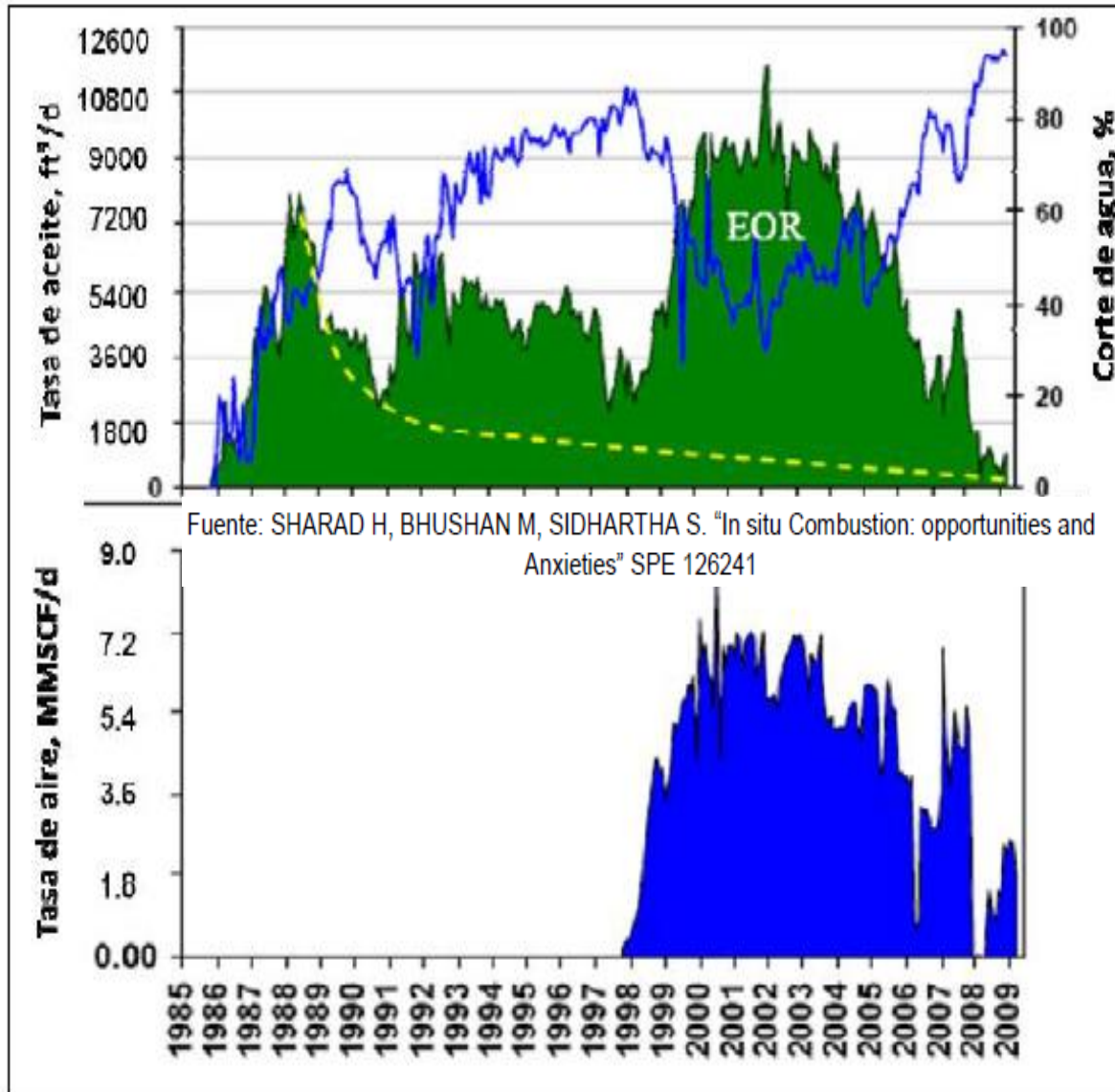


Balol and Santhal - Reservoir Properties

Field	Depth ft	Gross pay ft	Oil viscosity mPa.s	Permeability mD	Res. Pressure Initial / @ start of ISC (psi)	Observations
Suplacu de Barcau	115-720	27-290	2,000	5,000-7,000	140/80	
Balol	3280	10-95	100-450	3,000-8,000	1450/1450	Very strong edge water drive
Santhal	3280	16-195	50—200	3,000-5,000	1450/1450	
Bellevue	400	70/30	676	650	/40	

* Coal and carbonaceous material is present in the formation; sulphur content: 0.14

Desempeño del Campo Balol





Balol & Santhal: Results/Problems

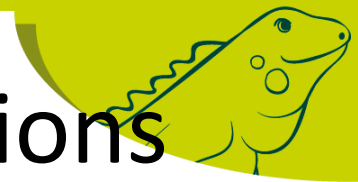
Results

- ❑ Ultimate oil recovery: >36%
- ❑ AOR 5,600 scf/bbl (1,000 sm^3/m^3)
- ❑ High inj. pressure: 1,500 psi (10.3 MPa)
- ❑ Average water cut: reduced from 70%-90% to 5-20%, due to ISC application (in some cases)
- ❑ Spontaneous ignition used for ISC initiation

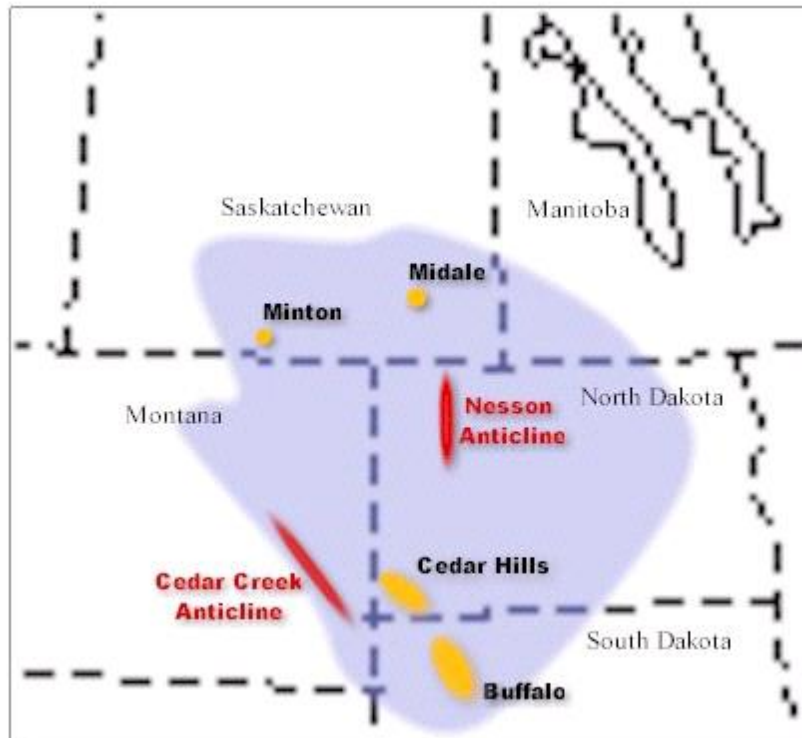
Operational Aspects

- ❑ Hot well workover challenges;
- ❑ Some H_2S is present in combustion gases, which are flared in tall flare stacks with outside make-up gases
- ❑ Challenges of operating separately two layers in the same stack

HPAI: Reported field applications



Williston Basin



www.northrim.sk.ca

- **Medicine Pole Hills Unit (MPHU)**

Secondary HPAI

Air injection started in 1987

- **Buffalo Red River Unit (BRRU)**

Secondary HPAI

Operations started in 1979

- **Horse Creek Field**

Secondary Air Injection started in 1996

Some published results

Others:

- **West Hackberry Field** - Louisiana

Tertiary Pilot in 1996

- **Handil Field** - Indonesia

Recent HPAI Pilot (2001)

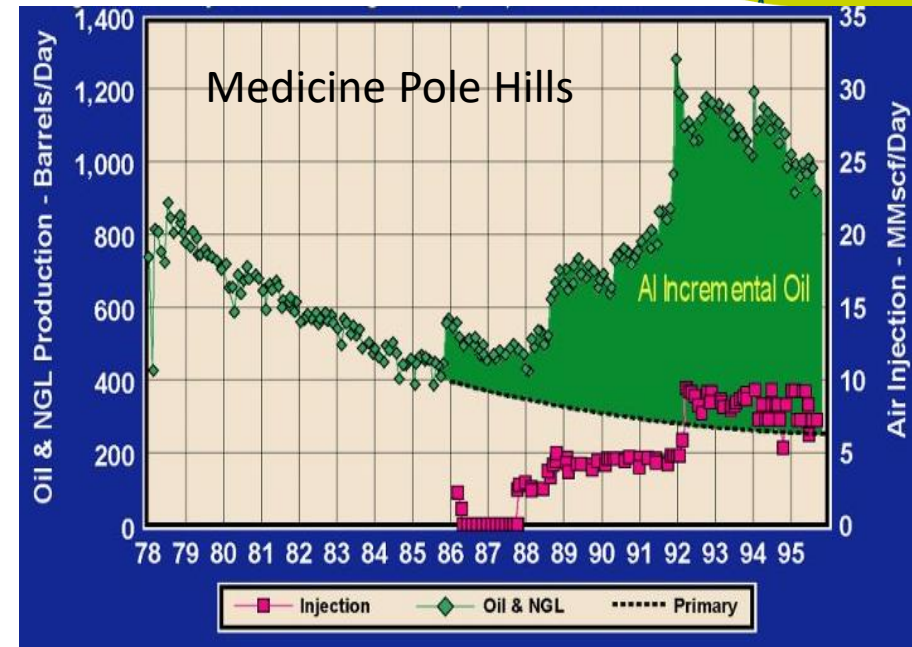
- **Barrancas Field** - Argentina (2005)

HPAI = High Pressure Air Injection in Williston Basin

- Tight limestone / dolomitic limestone
- Net Pay 10-18 ft
- Porosity 15-20%
- Sw around 50%
- Permeability 10 mD
- Reservoir pressure 3600 psi

Why Air injection?

- Water injectivity low (low perm, low water rel.perm) – needs high well density
- Air is cheap
- HPAI = flue gas drive (thermal contribution to RF is <25%)
- RF 18% on 160-320 Acre spacing



Cuenca Williston (EE.UU.): Petróleo Liviano

	Medicine Pole Hills	Buffalo Red River	Horse Creek
Formación	Red river	Red river	Red river
Zona productora	B y C	B	D
Profundidad	9500	8450	9125
Porosidad Promedio	B 19%, C 15%	20%	16%
Permeabilidad Promedio	B y C 5 md	10 md	10 y 20 md
Net pay promedio	18	10	20
GOR SCF/STB	525	120	205
Saturación de agua promedio	B 37%, C 48%	45%	35%
Temperatura de yacimiento °F	230	215	220
Presión inicial de yacimiento psi	4120	3600	4000
Gravedad API	39	30	32
OOIP	40,000,000	37,000,000	45,740,260
Factor de recobro primario %	15	5.95	9.92
Factor de recobro incremental %	14.25	15.67	16.62
Factor de recobro total %	29.25	21.62	26.53

Fuente: paper spe 38359

Field Case: HPAI vs Waterflood



Year	WBRRU			WBBRRU		
	Prim. (STB)	AI (STB)	Incr. (STB)	Prim. (STB)	WF (STB)	Inc. (STB)
1988	60,992	102,986	41,994	61,868	50,118	(11,750)
1989	53,796	146,187	92,391	52,785	49,441	(3,344)
1990	46,623	159,297	112,674	43,508	51,679	8,171
1991	37,234	170,067	132,833	37,339	54,045	16,706
1992	31,906	158,013	126,107	30,525	57,660	27,135
1993	24,851	133,579	108,728	26,411	82,661	56,250
1994	21,588	124,671	103,083	22,902	112,541	89,639
1995	16,849	118,380	101,531	18,671	117,723	99,052
1996	12,238	113,839	101,601	15,133	99,958	84,825
1997	10,175	126,817	116,642	12,450	99,057	86,607
1998	9,269	122,165	112,896	10,914	86,225	75,311
1999	7,301	110,171	102,870	8,440	81,695	73,255
2000	4,831	98,869	94,038	6,915	79,282	72,367
2001	3,264	102,025	98,761	4,461	75,966	71,505
2002	2,100	94,550	92,450	2,946	73,102	70,156
2003	1,949	87,907	85,958	2,079	68,653	66,574
2004	0	75,140	75,140	1,920	70,522	68,602
2005	0	136,409	136,409	0	69,759	69,759
TOTAL	344,966	2,181,072	1,836,106	359,267	1,380,087	1,020,820
RF (%)	1.2	7.5	6.3	1.7	6.7	5.0

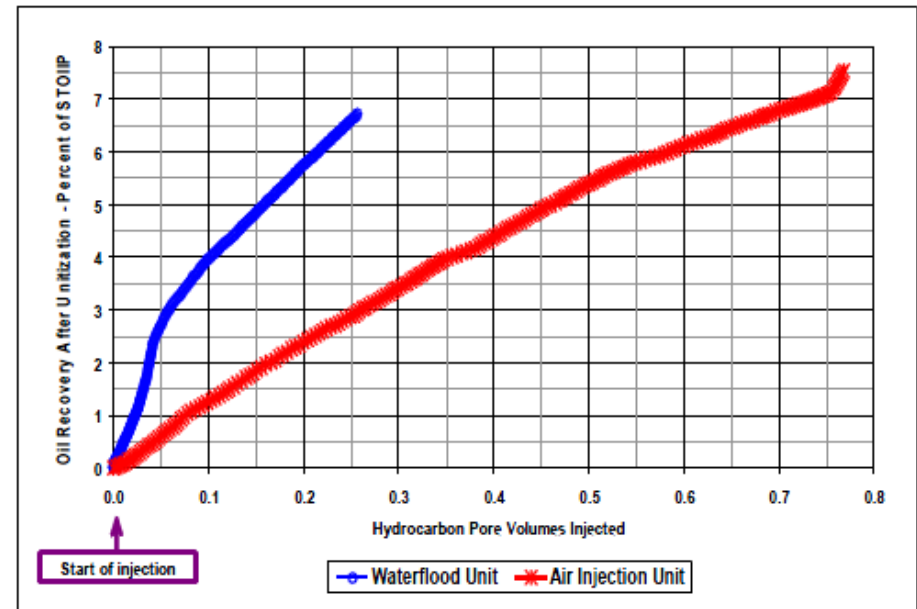


Fig. 11 Displacing Efficiency

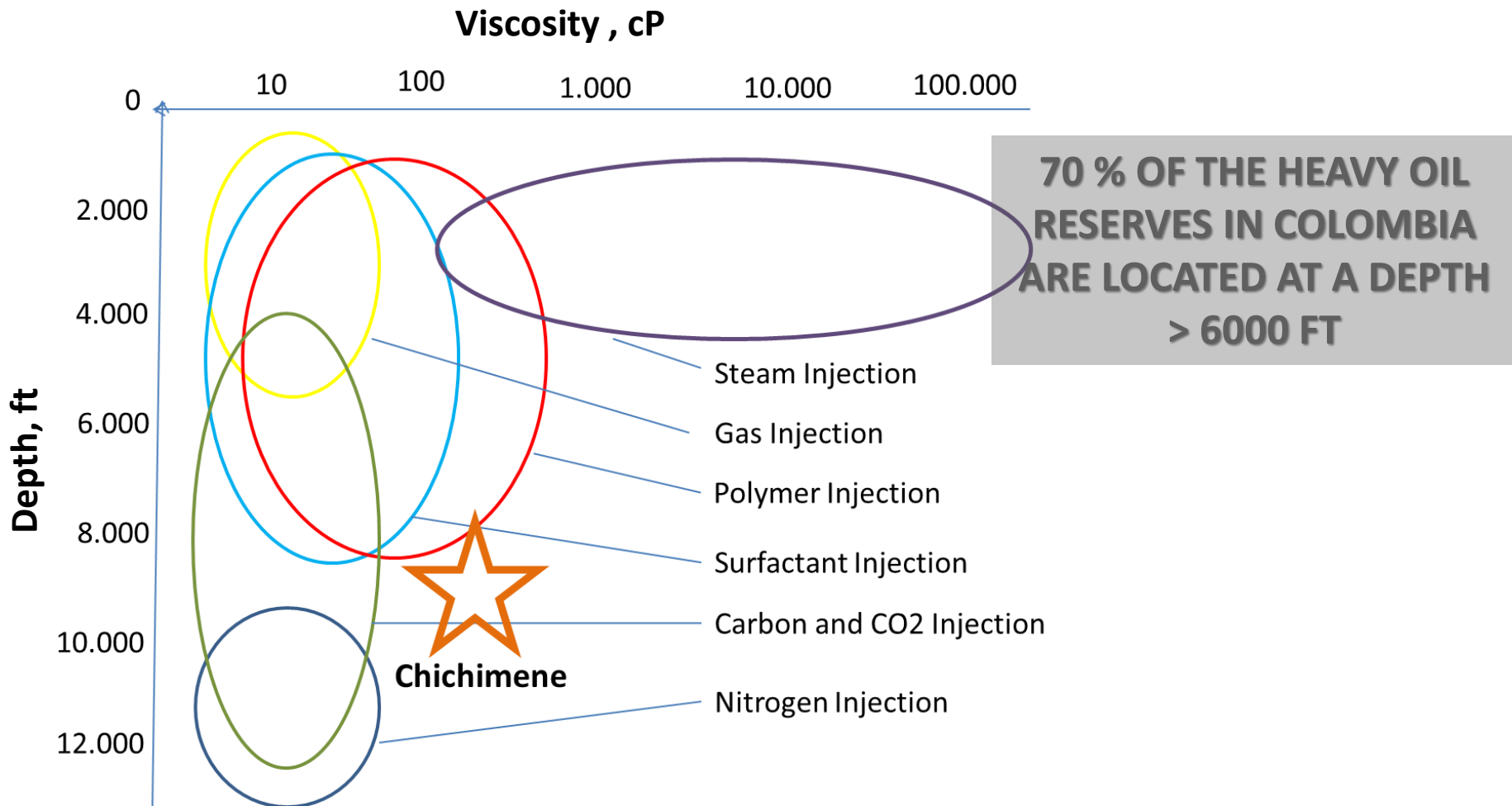
SPE 99454: Air Injection and Waterflood Performance Comparison of Two Adjacent Units in Buffalo Field: Technical Analysis

V.K. Kumar, D. Gutiérrez, G. Moore, S. Mehta



PILOTO DE INYECCIÓN DE AIRE EN CHICHIMENE

Why In situ Combustion in Colombia?

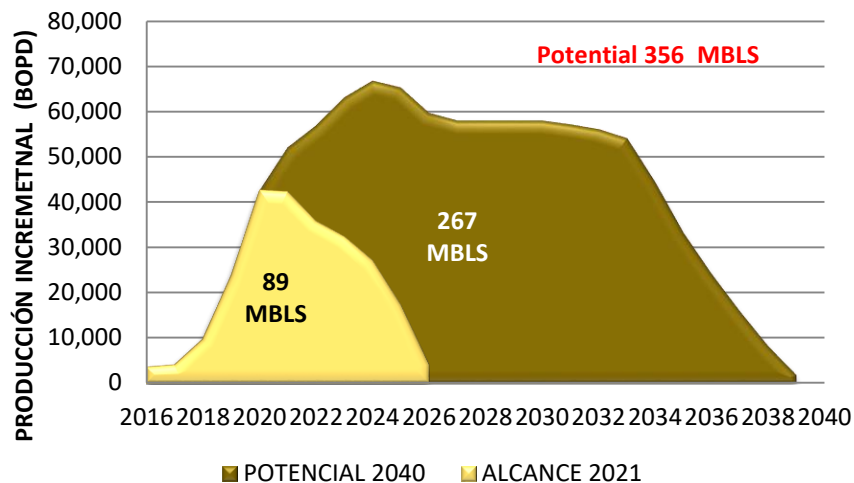


Source: Enhanced Oil Recovery (EOR) Report, Royal Dutch Shell.

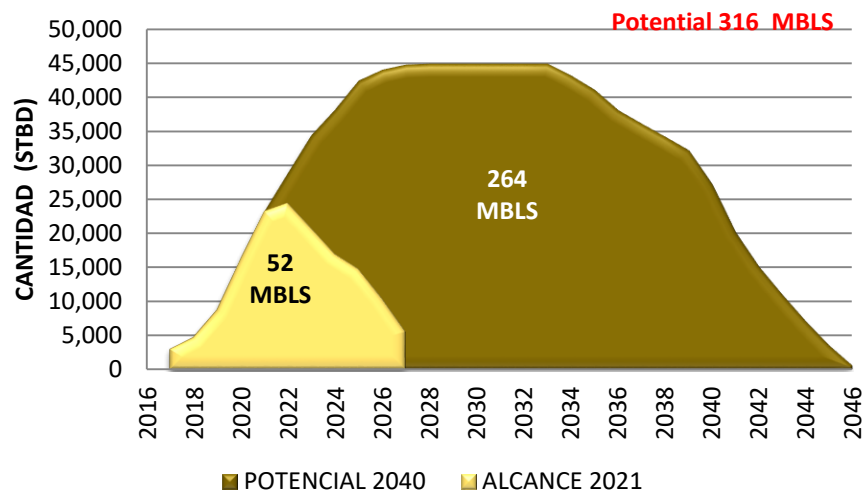
PRODUCTION FORECAST - EXPANSIONS



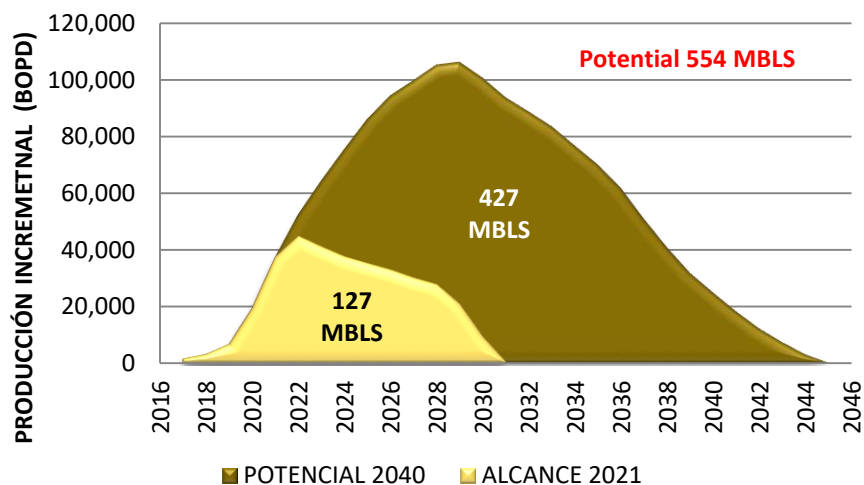
CHICHIMENE



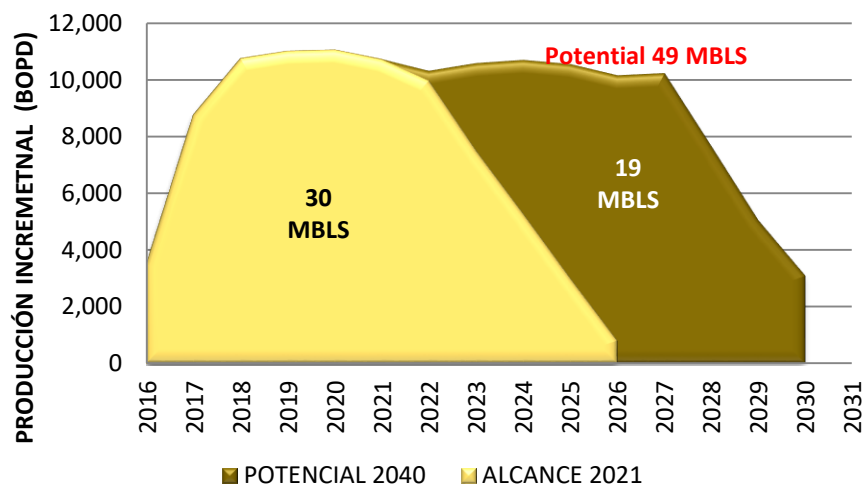
CASTILLA



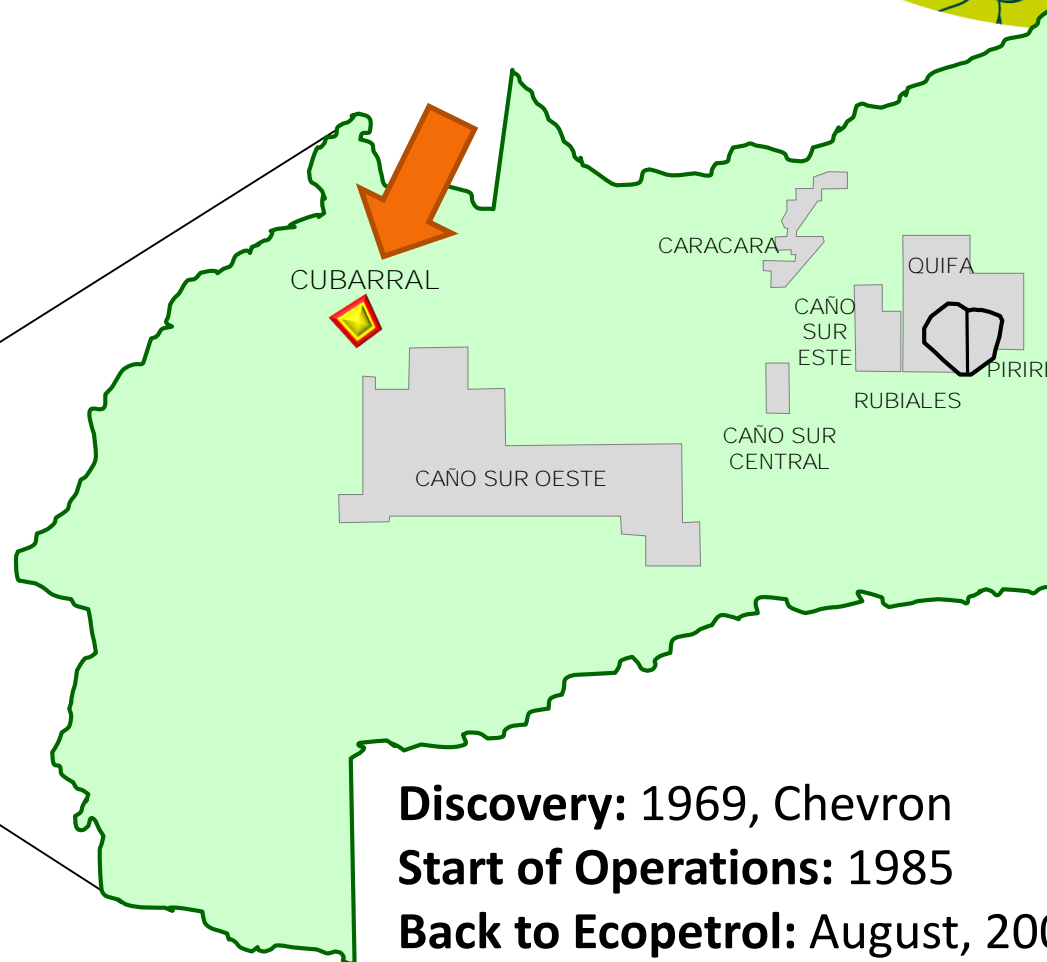
RUBIALES



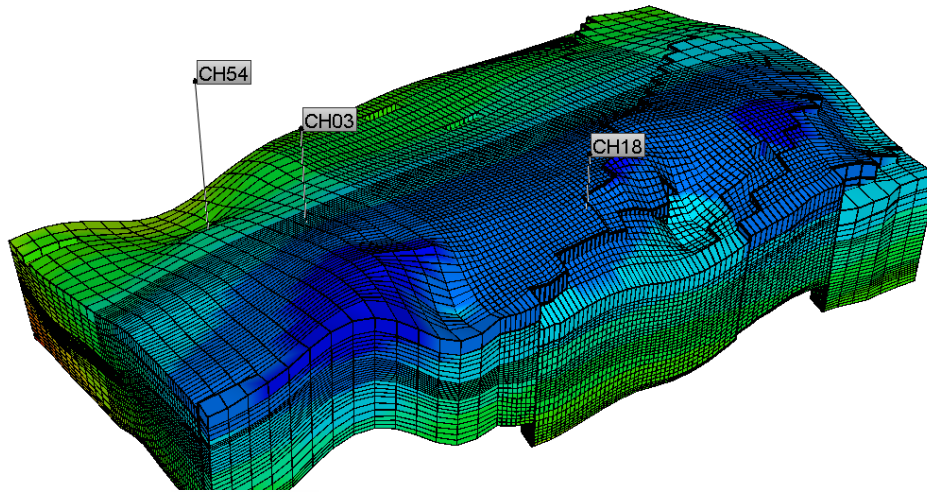
CAÑO SUR



Chichimene Field



Discovery: 1969, Chevron
Start of Operations: 1985
Back to Ecopetrol: August, 2000
Current Production: 80,000 bpd
Steep Pressure Decline
Primary UER ≈ 9%



Allied with world-class strategic partners, Ecopetrol has acquired skills and capacities for ISC physical and numerical modeling for extra-heavy oil reservoirs.



AT EOR CONSULTING INC
Alex Turta



Combustion Tube Reactor

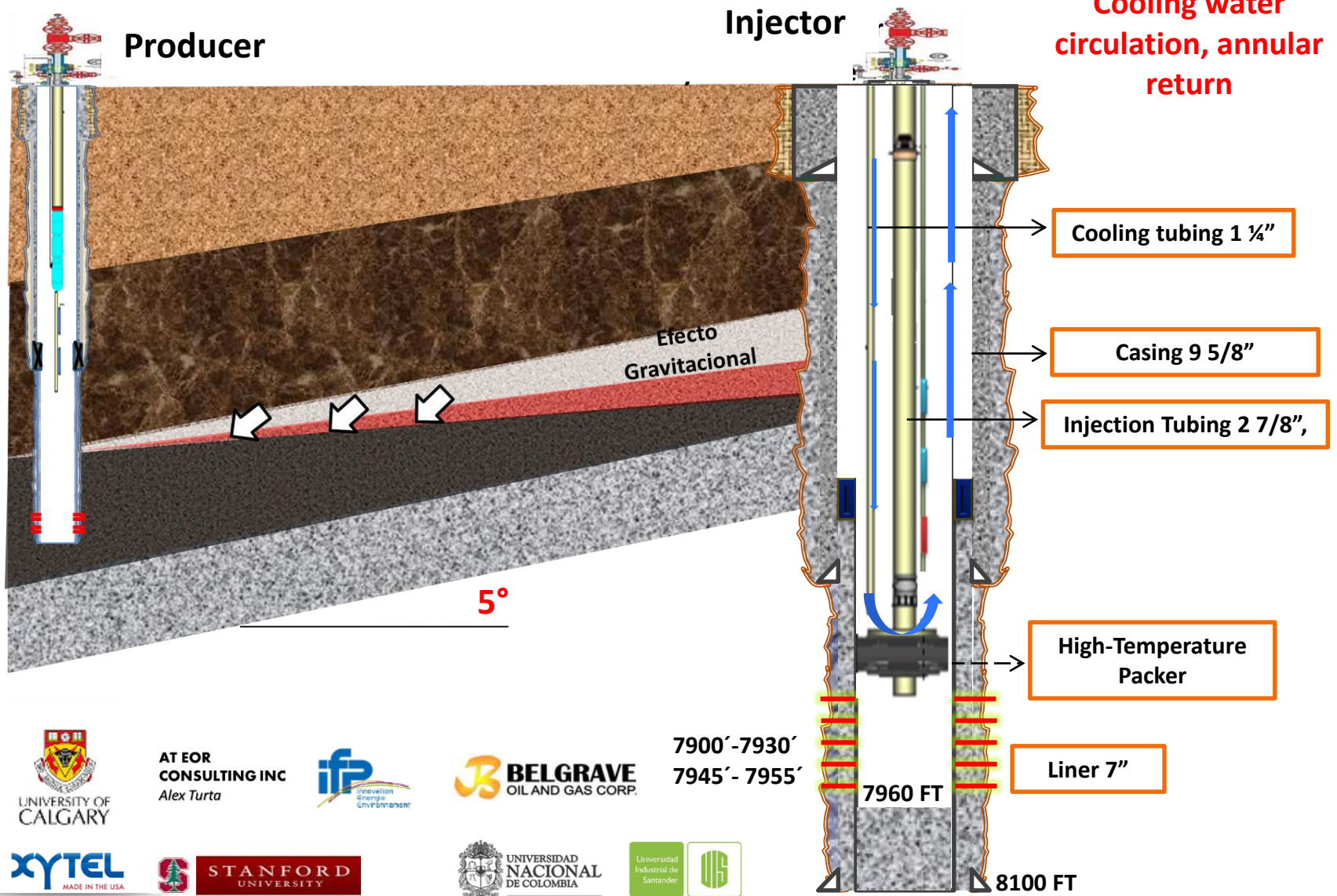


RTO Kinetics Cell



Isothermal Cell

Eco-GSAI[®] Pilot Design (Gravity-Stabilized Air Injection)



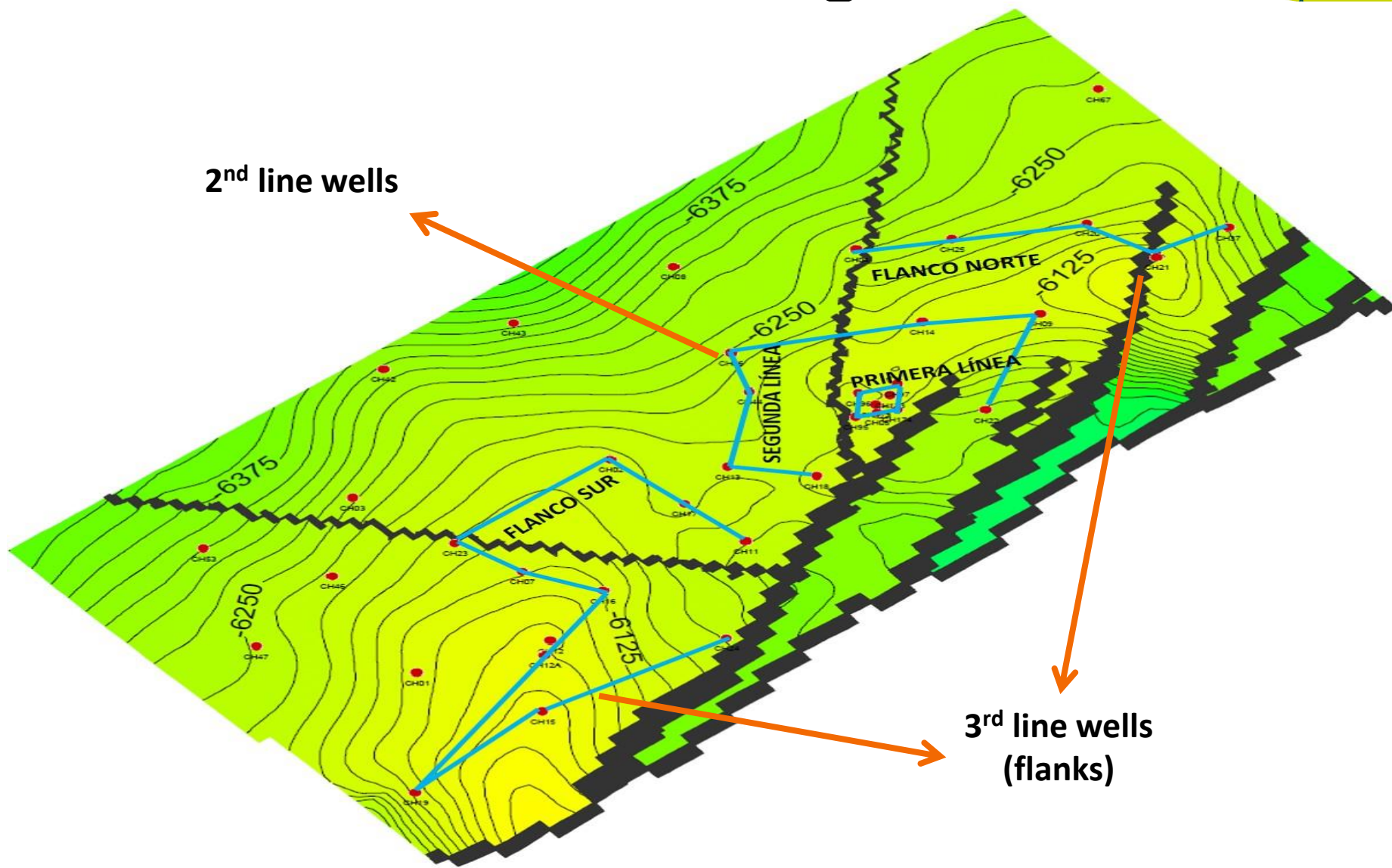
AT EOR CONSULTING INC
Alex Turta



7900' - 7930'
7945' - 7955'



Pilot Design



2nd line wells

3rd line wells
(flanks)

Pilot Premises



Able to prove the technology concept for deep, extra-heavy oil reservoirs

Evaluation time of 2 years is sufficient

Ultimate RF of 35% OIIP is possible

Project Timeline



2012-2014: Construction of own ISC laboratory and equipment, Pilot detailed design



Before 2011: Screening, preliminary lab tests, kinetics model, ISC world survey, People assignment (40+ professionals)



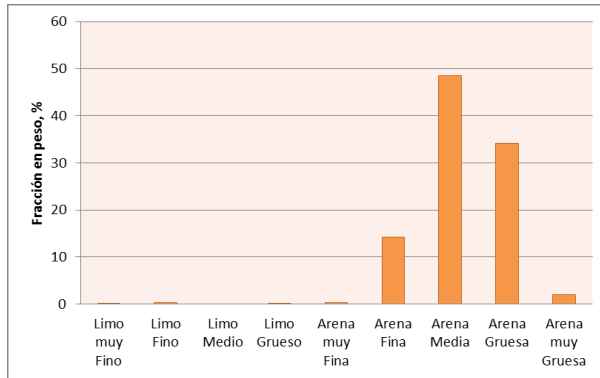
2015-2017: Construction of field facilities, Detailed lab tests, Connectivity test, Ignition



Reactivity Studies: Core vs. Outcrop

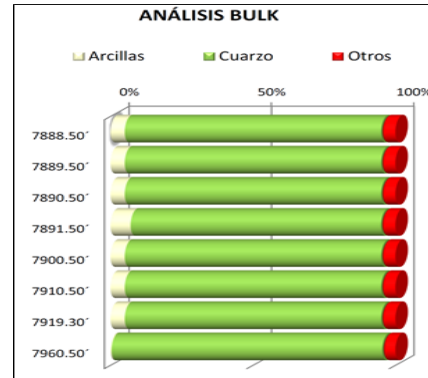


Particle size distribution

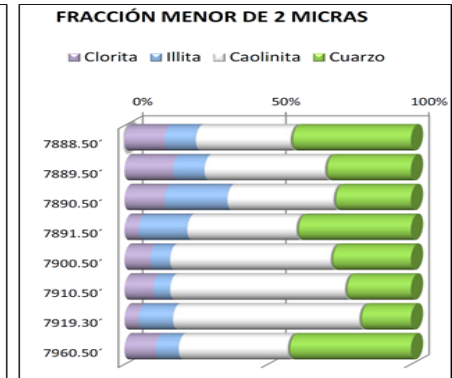


Core

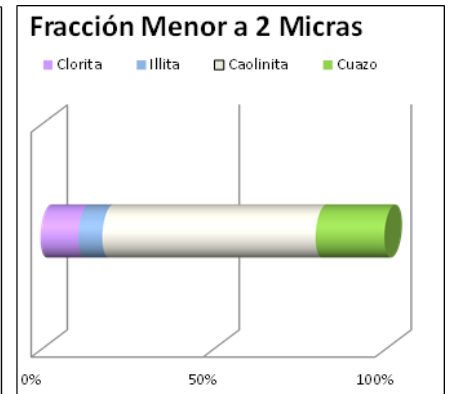
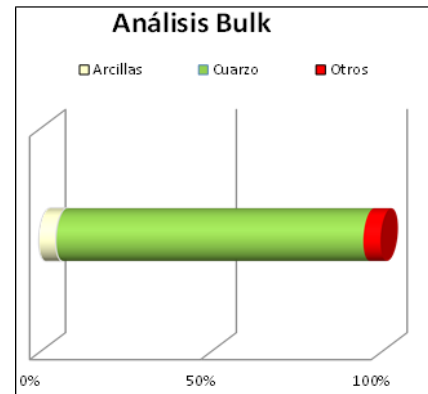
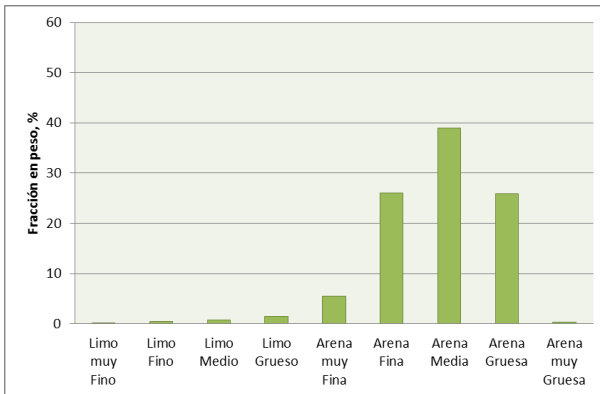
Bulk Composition



Clay Composition



Outcrop

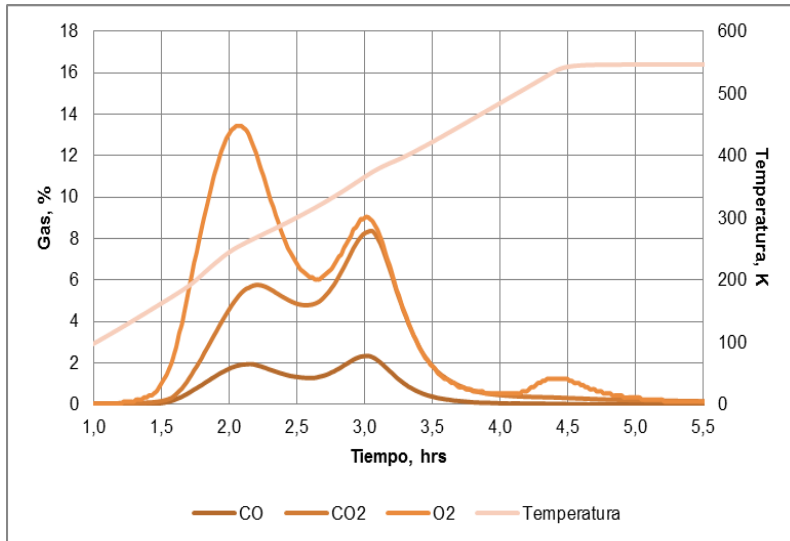


TRUJILLO, M.: EVALUACIÓN DE LA INFLUENCIA DE LA MATRIZ DE LA ROCA EN LA CINÉTICA DE LA COMBUSTIÓN PARA EL PROCESO DE INYECCIÓN DE AIRE EN CRUDOS PESADOS. Master of Science Thesis, Universidad Industrial de Santander, Colombia, 2015.

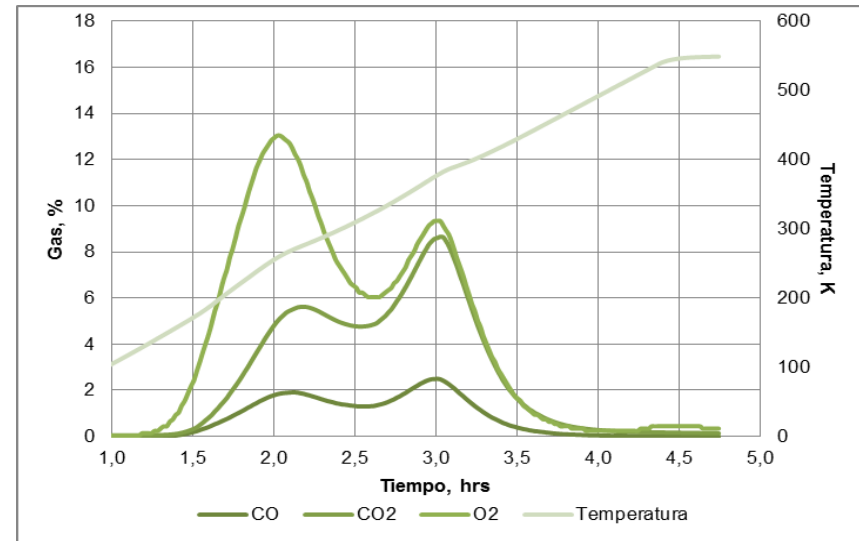
Reactivity Studies: Core vs. Outcrop



Core



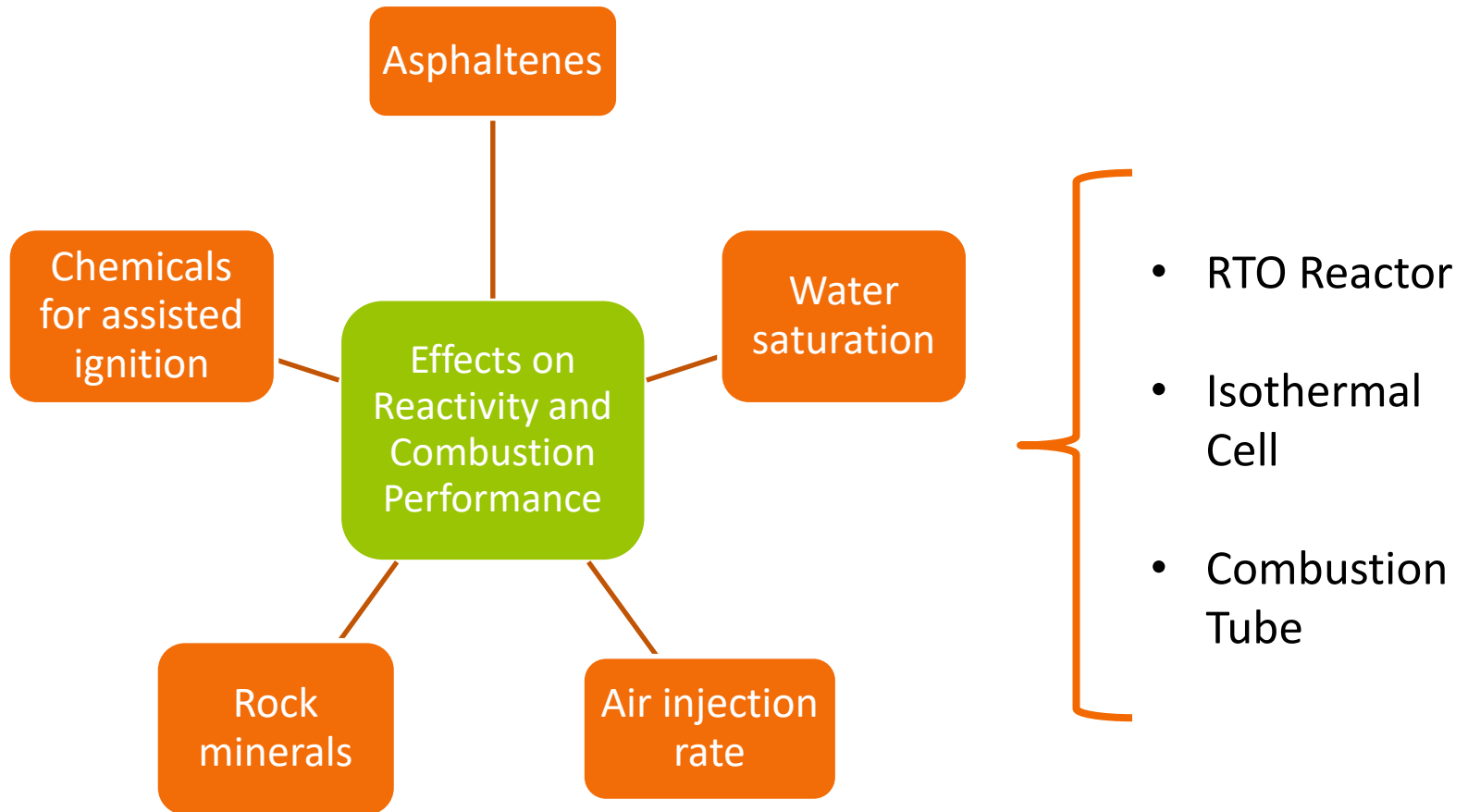
Outcrop



- The outcrop samples compositionally resemble the reservoir rock
- Their reactivities are also comparable
- This means using the outcrop rock for RTO and combustion test studies is feasible
- It results in significant cost savings
- Enables experimental studies to evaluate the effect of reservoir and operating parameters on reactivity and combustion performance



Experimental Studies at the ISC lab



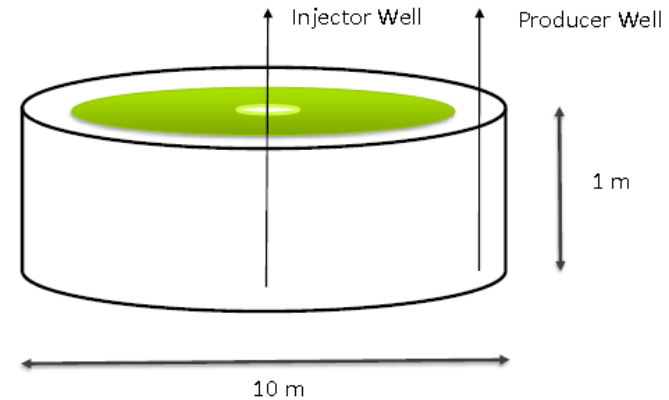
Ignition Study



(Ignition Evaluation of In-Situ Combustion Process of Chichimene Field, *H. Bottia*, M. Aguillón, H. Lizcano, C. Delgadillo, C. Gadelle, ThEOR 2016, Kazan, Russia)



Isothermal Cell Experiments



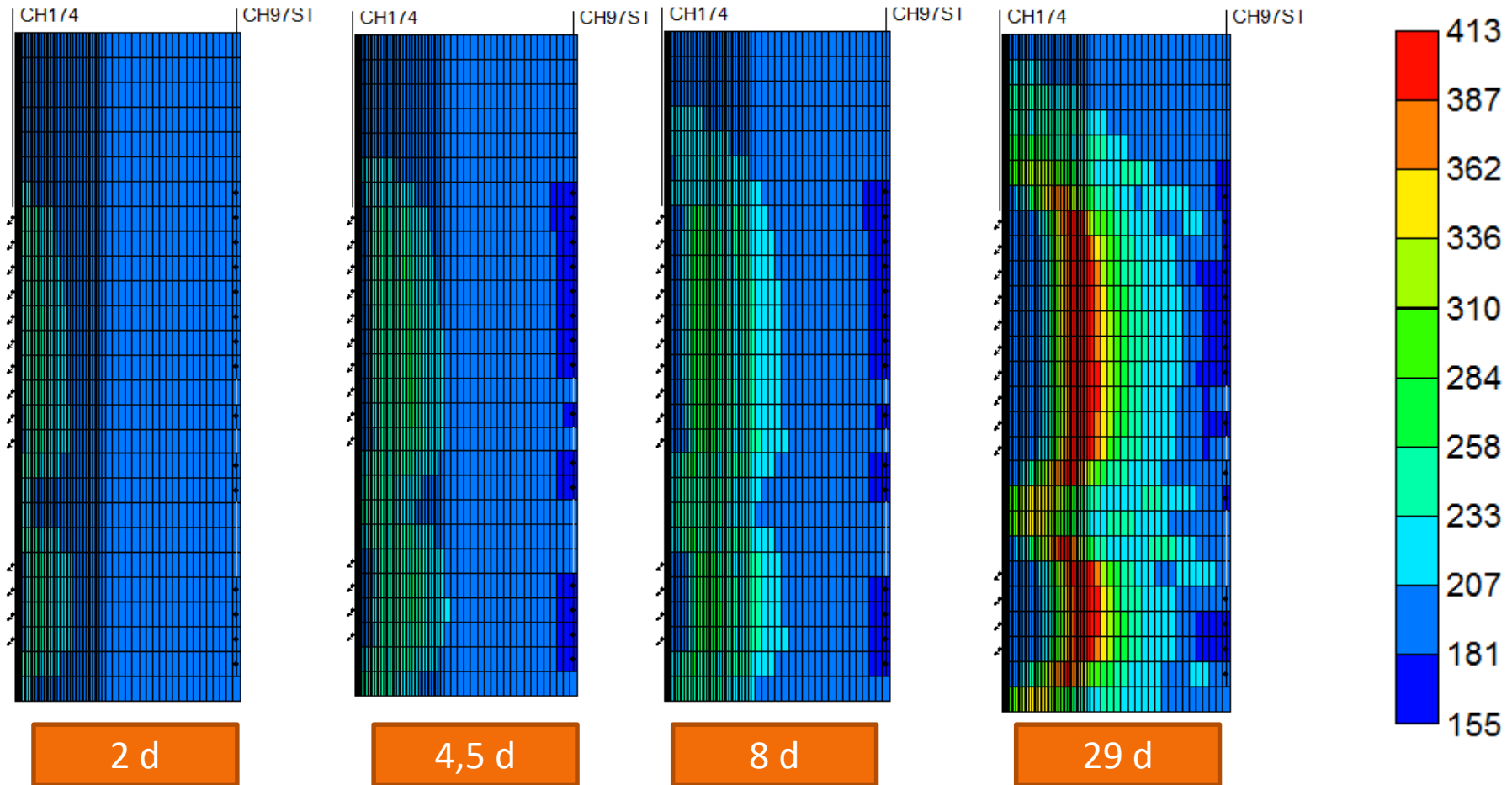
Analytical & Numerical Modeling

- Ignition delay \approx 2 days
- Ignition distance \approx 2 m

High Resolution Radial Model (Ignition)



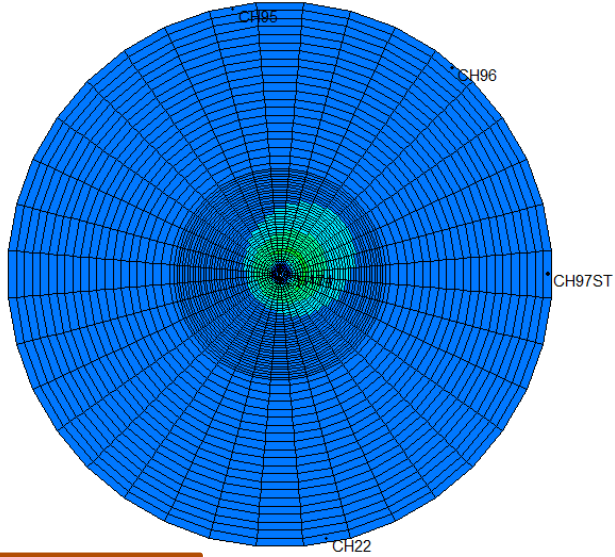
Results:



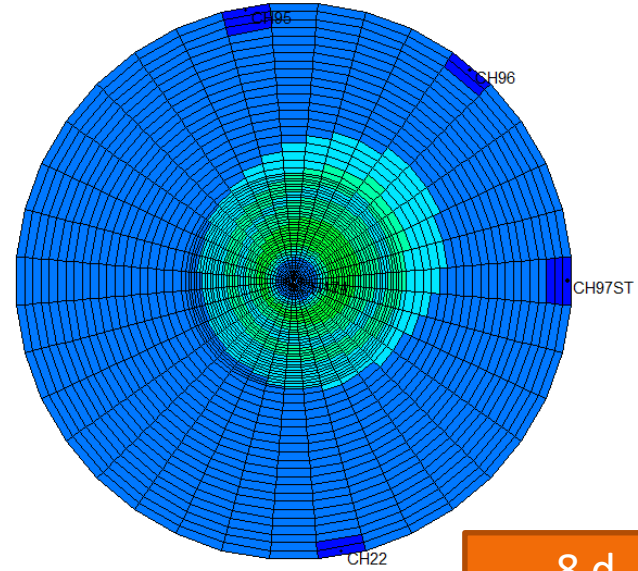
High Resolution Radial Model (Ignition)



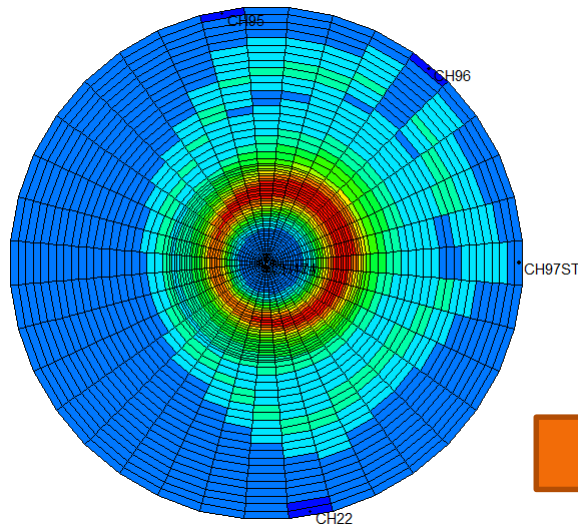
Results:



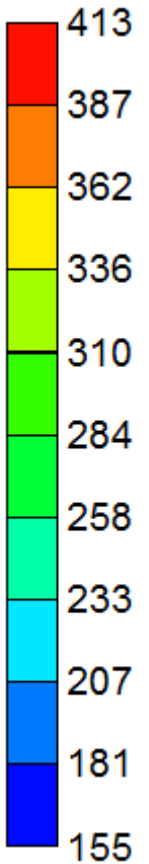
2 d



8 d



29 d



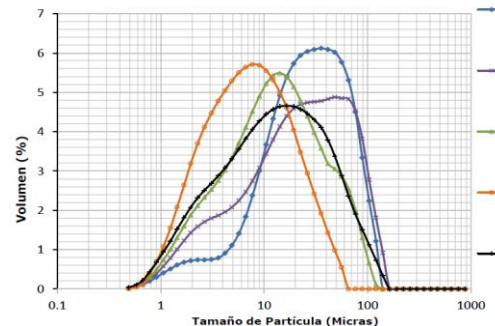
Experimental Study: Emulsions



Produced oxidized crude oil in a continuous flow reactor (Patent pending)

Create synthetic emulsions.

They are comparable with analogue field produced emulsions



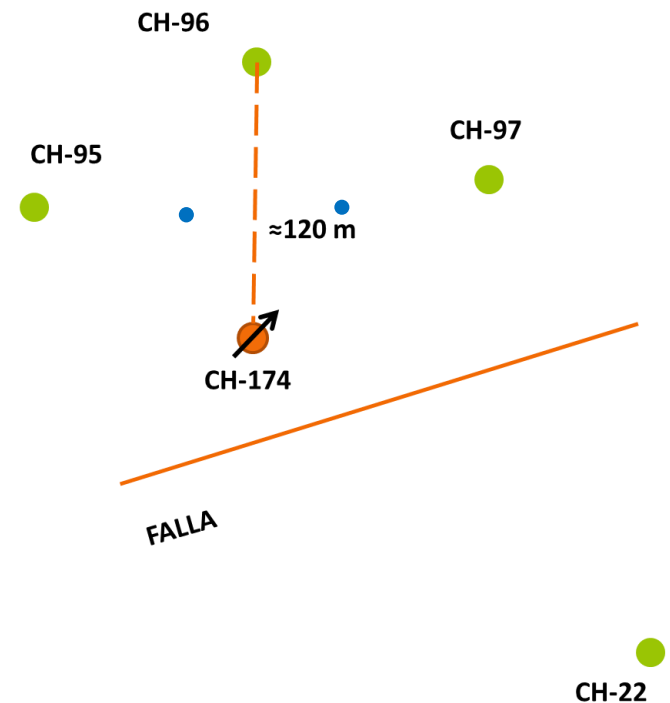
Proactively studying alternatives for effective treatment: Chemical, dilution, thermal, combined.



Nitrogen Connectivity Test




- Objectives:
 - Test if any preferential direction for gas flow exists
 - Dimension the residence time of the combustion gases in the pilot area
 - Test the response of the artificial lift system to increased GOR
 - Update the simulation model






Connectivity Test Development

ES pumps had a hard time with high GORs. The wells were eventually shut in

 N₂ broke through between days 8-10 at the 1st line wells

 Injection continued for almost 30 days. N₂ was measured in almost all of the 2nd line wells and some 3rd line wells.



How are we for ISC?

Challenges:

Oxygen Production

High reactivity at reservoir T

**Transit time (8 d)
longer than ignition
delay (2 d)**

Emulsions

Proactively preparing a response for treatment

Artificial Lift

Fewer options at 8,000 ft deep, extra-heavy oil, high GOR

Optimizing ESP design for expected rates and GORs.

Next Steps



- Deploy the artificial lift solution
- Predict the ignition performance based on the updated simulation model
- Make slight adjustments to treatment facilities to allow for flexible emulsion treatment
- Adjust the monitoring plan for ignition and steady air injection
- Continue with the experimental efforts to support the operation before any deviation



Challenges and Future Activities

- Predictive modeling of ISC at field scale (Stanford)
- Nano-catalysts for promoting ignition
- Finishing “base lines” and measuring deviations
- Operate the pilot with minimal disturbance
- Extrapolate the pilot findings to the field scale
- Deal with hot well operations (expansion)
- Cost reduction (lower-grade metallurgy, fluid treatment, compressor reliability)
- Environmental (Emissions, flue gas use, water quality)

Acknowledgments



- The laboratory, operations and reservoir Chichimene ISC team, both at the Colombian Petroleum Institute and other areas of Ecopetrol
- Our team of partners and consultants throughout the stages of the project: Alex Turta, Claude Gadelle, Louis Castanier, Olivier Clause, John Belgrave, Antony Kovscek, Margot Gerritsen, Marco Thiele, Gordon Moore, Raj Mehta, ONGC





Para uso restringido en Ecopetrol S.A. Todos los derechos reservados. Ninguna parte de esta presentación puede ser reproducida o utilizada en ninguna forma o por ningún medio sin permiso explícito de Ecopetrol S.A.

